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Optimization of flow state for the control of the reduction-oxidation reaction

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Collaborative work with Prof. Dr. Dieter Bothe (TU Darmstadt)

Outline

1. Self-introduction – Applied physical chemistry

- Electrochemistry and its applications
- Fluid dynamics and Electrochemistry
- 2. Motivation for main topic Nanoparticles
 - What is nanoparticles ?
 - Objective of this research
- 3. Strategy for process optimization
 - Fundamental concept
 - Strategies for process optimization

Introduction of Applied Physical Chemistry lab.

Our research topic

- Development of new devices using Electrochemistry
- Elucidation of phenomena in Electrochemistry

Device Development



* H. P. Nguyen et al, Electrochimica Acta 68, 9-12 (2012).

Introduction of Applied Physical Chemistry lab.

Our research topic

- Development of new devices using Electrochemistry
- Elucidation of phenomena in Electrochemistry

Phenomena Understanding



Electrochemistry

Electrochemistry

Subject of Reduction/Oxidation (Redox) reaction occurring at (Solid-Liquid) Interface

Redox reaction

ightarrow External power source controls the reaction behavior

[Reaction at Interface]

- \rightarrow State of interface should be well understood
- → Both reaction at the interface and $\frac{\text{transport toward the interface}}{\downarrow}$ should be well considered

Fluid Dynamics enormously contribute to Electrochemistry

Fluid Dynamics provide the method to control transport behavior of reactants in electrochemistry



Diffusion behavior of reactant determines the rate of electrochemical phenomena

Fluid Dynamics provide the method to control transport behavior of reactants in electrochemistry



How to control the diffusion behavior ??













Fluid Dynamics provide the method to control transport behavior of reactants in electrochemistry



Fluid Dynamic solution controls the rate of electrochemical reaction

T. von Karman, *Z. Angew. Math. Mech.*, **1**, 233 (1921).

W. G. Cochran, Proc. Cambridge Philos. Soc., 30, 364 (1934).,

V. G. Levich, "Physicochemical Hydrodynamics", Prentice-Hall, Englewood Cliffs, NJ (1962). 4

Electrochemistry

Subject of Reduction/Oxidation (Redox) reaction occurring at (Solid-Liquid) Interface

Fluid Dynamics enormously contribute to Electrochemistry

Using Fluid Dynamics efficiently

Building finer electrochemical processes

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Nanoparticle

Nanoparticle ••• Nano-size structure with diameter 1 – 10, 100 nm, which shows totally different characteristics from bulk structure

Application ••• Electronic devices, Medical systems, Cosmetics, etc.



- I . Size (diameter) and its distribution \rightarrow Minimizing the distribution of size
- II. Crystallinity → Customizing crystallinity
- III. Composition \rightarrow Customizing composition



- I. Size (diameter) and its distribution
 - → Providing simultaneous nucleation and nuclear growth with same speed
- II. Crystallinity
 - Providing stable
 and calm nuclear growth
- III. Composition
 - \rightarrow Optimizing reactant composition

I. Size (diameter) and its distribution

- → Providing simultaneous nucleation and nuclear growth with same speed
- II. Crystallinity
 - \rightarrow Providing stable

and calm nuclear growth

Focused !!

III. Composition

 \rightarrow Optimizing reactant composition

Directionalities

Using micro-reactor (2 inlets/ 1 outlet)

T-shaped

Y-shaped



Using optimized flow and reaction in the reactor

Target



Co (Cobalt) nanoparticles for magnetic recording media

Creating particle by Redox reaction in T-shaped reactor

Creating particle by Redox reaction in T-shaped reactor



Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻



Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻



Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻



Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻





Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻



Creating particle by Redox reaction in T-shaped reactor

Reducing agent: H₂PO₂⁻



- Factors we trying to control and the way to control
 - I. Size (diameter) and its distribution
 - → Providing simultaneous nucleation and nuclear growth with same speed
 - II. Crystallinity
 - \rightarrow Providing stable
 - and calm nuclear growth



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Strategy No. 1



A few flow types at the junction part



Merit of "vortex flow"



Merit of "vortex flow"

Nucleation



Reaction field for Redox reaction

is concentrated

Efficient and simultaneous nucleation is realized



Strategy No. 2



Inject solutions with adequate *Re and surface modification for the channel wall,* generating "symmetric laminar" flow
Merit of moderate Re

Flow transition of vortex flow in reactor



Vortex flow system can really provide stable field ??

Asymmetric laminar flow



Vortex flow system can really provide stable field ??

Asymmetric laminar flow



Additional force (vertical to the wall)

disturbing particle trajectory works for growing particle



S. Fukuoka et al., *土木学会論文報告集*, 295, 31 (1980).,18

Vortex flow system can really provide stable field ??

Symmetric laminar flow



Symmetric laminar flow



Growing field becomes stable

Adequate *Re* of solution and surface modification needed

Symmetric laminar flow



Details about the particle movement should be analyzed by Euler/Lagrange equation

Strategy No. 3



How to deal with additional nucleation in the growth step ?

Adding "sulfuric additives", promoting surface reaction of reductant

Effect of sulfuric additive



J. Kivel et al., J. Electrochem. Soc., **112**, 1201 (1965)., **20**



Analysis of the effect of additives on metal (Ni) surface, using Quantum Chemistry (QM) simulation technique

 $\hat{H}\Psi = E\Psi$

Solving Schrödinger eq. for electrons of the system

= H

= C



Accelerating mechanism of thiourea

Thiourea adsorbs on metal surface



Accelerating mechanism of thiourea

Neighbor part becomes positive after the electron move e

Accelerating mechanism of thiourea



Adsorption of anion reductant, H₂PO₂⁻, is enhanced by additive



Reaction of
$$H_2PO_2^{-1}$$

 $H_2PO_2^{-1} + 2OH^{-1} \rightarrow$
 $H_3PO_4^{-1} + H_2O + 2e^{-1}$

is promoted by additive

On Metal >> In Solution

Suppress new nucleation in the growth step part

Strategy No. 4



How to analyze the flow state and the reaction behavior ?



Using "CFD simulation" and "QM simulation"

Quantum Mechanics (QM) simulation

Capability of QM simulation



Capable to evaluate reactivity, reaction rate, physical stability

Concept of methodology

Analysis system of the research



Actual process

Nanoparticle synthesis using Y-shaped reactor



Nanoparticle synthesis using Y-shaped reactor

Description of micro-reactor system



Tentative results

CoPt nanoparticle



Aggregation of particles and size distribution are observed



Summary

Objective

Control of Size and its distribution of Nanoparticles Crystallinity

Methodology

Redox reaction in T or Y-shaped micro-reactor

Strategies

Simulations $\overrightarrow{}$ Synthesis/Measurement

Moderate Re, Modified surface, Designed additive

(i) Vortex flow (at junction part)(ii) Symmetric Laminar flow (at channel part)(iii) Promoted Redox reaction on the particle surface

Acknowledgement

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<u>コアシェル構造金属ナノ粒子の合成</u>

微小流路内へ二液を同時に導入した際に形成される液-液 界面を用いて反応を試みた.



マイクロ流路系のモデル化一基礎式

$$\partial_t \theta_i - \nabla \cdot (D_i^{surf} \nabla_{\Sigma} \theta_i^{mol,\Sigma}) = \mathbf{j}_i^{mol} \cdot \mathbf{n} + R_i^{\Sigma}$$



 \mathbf{j}^{mol} :モル流速 R:正味の反応速度 r^{gen} :生成反応速度 r^{count} :逆反応速度 r^{ad} :吸着速度 r^{de} :脱離速度 θ :表面被覆率(面濃度) D_i^{surf} :表面拡散係数

マイクロ流路系のモデル化一基礎式

$$\frac{\partial_{t}\theta_{i}}{\mathbf{v}} - \nabla \cdot (D_{i}^{surf} \nabla_{\Sigma} \theta_{i}^{mol,\Sigma}) = \mathbf{j}_{i}^{mol} \cdot \mathbf{n} + R_{i}^{\Sigma}$$

$$\frac{\partial_{t}\theta_{i}}{\mathbf{v}} - \nabla \cdot (D_{i}^{surf} \nabla_{\Sigma} \theta_{i}^{mol,\Sigma}) = \mathbf{j}_{i}^{mol} \cdot \mathbf{n} + R_{i}^{\Sigma}$$

$$\mathbf{j}_{i}^{mol} \cdot \mathbf{n} = r_{i}^{ad,\Sigma} - r_{i}^{de,\Sigma}$$

$$\mathbf{j}_{i}^{mol} = \mathbf{u} \cdot c_{i} - D_{i} \nabla c_{i}$$

$$R_{i}^{\Sigma} = r_{i}^{gen,\Sigma} - r_{i}^{count,\Sigma}$$

$$r^{\Sigma} = k \prod_{k} \theta_{k}^{n_{k}}$$

仮定 その3)

<u>ナノ粒子上の吸着子の被覆率は</u> <u>定常状態にあると近似することができる</u>

マイクロ流路系のモデル化ー基礎式

$$\frac{\partial_{t} \theta_{i}}{\mathbf{y}} - \nabla \cdot (D_{i}^{surf} \nabla_{\Sigma} \theta_{i}^{mol,\Sigma}) = \mathbf{j}_{i}^{mol} \cdot \mathbf{n} + R_{i}^{\Sigma}$$

$$\mathbf{j}_{i}^{mol} \cdot \mathbf{n} = r_{i}^{ad,\Sigma} - r_{i}^{de,\Sigma}$$

$$\mathbf{j}_{i}^{mol} = \mathbf{u} \cdot c_{i} - D_{i} \nabla c_{i}$$

$$R_{i}^{\Sigma} = r_{i}^{gen,\Sigma} - r_{i}^{count,\Sigma}$$

$$r^{\Sigma} = k \prod_{k} \theta_{k}^{n_{k}}$$

仮定 その4)

<u>ナノ粒子上の吸着子の表面拡散は</u> 他の事象と比較して遅く無視してよい

マイクロ流路系のモデル化ー基礎式

$$\frac{\partial_{i}\theta_{i}}{\mathbf{y}} - \nabla \cdot (D_{i}^{surf} \nabla_{\Sigma} \theta_{i}^{mol,\Sigma}) = \mathbf{j}_{i}^{mol} \cdot \mathbf{n} + R_{i}^{\Sigma}$$

$$\mathbf{j}_{i}^{mol} \cdot \mathbf{n} = r_{i}^{ad,\Sigma} - r_{i}^{de,\Sigma}$$

$$\mathbf{j}_{i}^{mol} = \mathbf{u} \cdot c_{i} - D_{i} \nabla c_{i}$$

$$R_{i}^{\Sigma} = r_{i}^{gen,\Sigma} - r_{i}^{count,\Sigma}$$

$$r^{\Sigma} = k \prod_{k} \theta_{k}^{n_{k}}$$

$$\mathbf{j}_{i}^{mol} \cdot \mathbf{n} = -R_{i}^{\Sigma}$$
暫定的な基礎式の導出

ディスカッション内容-②核発生段階の考え方

<これまでの大まかな考え方 [一段階式]> 還元剤と金属イオンが反応して粒子核が発生



ディスカッション内容-③新しい方針

前方針の欠点:発生した核がおかれる速度場が乱雑

→ 核成長の度合いに差

→ 粒径制御への寄与 小

議論を通しての改善策: vortex flow の適用

vortex flow の利用



- → ①反応物の接触場をchannel中心に集中
 - ② 層流による安定した一様な核成長場の実現
- → ① 同時的で一様な反応場の実現
 ② 一様な核成長場の実現





- → vortex flow をつくるための条件の最適化
 - simulation software OpenFOAMの利用
 - ・実験による粒径分布の計測

量子化学計算の応用

物質収支式(移流,拡散,反応)

$$\partial_t c_i + \mathbf{u} \cdot \nabla c_i = \nabla \cdot (D_i \nabla c_i) + r_i$$

i:反応種 c:濃度 \mathbf{u} :速度ベクトル D:拡散係数

r:反応による濃度変化速度(反応速度)

Y → <u>量子化学計算による算出</u> **反応流体の挙動のメカニズム解明へ**

量子化学計算の他の側面

- 量子化学計算で他に何ができるのか?
- ☆ 量子化学計算で算出可能な種々のパラメータ
 - (1) 平衡状態における分子のエネルギー
 - (2) 基準振動の波数
 - (3) 分子の電荷分布, 双極子モーメント
 - (4) 分子のエントロピー, エンタルピー, ギブズ自由エネルギー ((1), (2)から)
 - (5)反応の遷移状態における(1)~(4)パラメータ((2)から) etc.
- 活性錯合体理論に基づく反応速度定数 k

$$k = B \exp\left(-\frac{\Delta^{TS} G^{\circ}}{RT}\right)$$

B: (分子の運動速度, トンネル効果を考慮した補正因子等を全て含んだ因子) $\Delta^{TS}G^{\circ}$: 始状態に対する遷移状態のギブズエネルギー R:気体定数 T:温度

量子化学計算の他の側面

対流·拡散·反応方程式

$$\partial_t c_i + \mathbf{u} \cdot \nabla c_i = \nabla \cdot (D_i \nabla c_i) + r_i$$

i:反応種 C:濃度 \mathbf{U} :速度ベクトル D_i :拡散係数

$$r_i = k_a \prod_k c_k^{n_k} - k_b \prod_l c_l^{n_l}$$

 k_a : i 種生成反応速度定数(次数は $\sum_{k} n_k$) k_b : i 種生成反応速度定数(次数は $\sum_{l} n_l$)

量子化学計算によって反応項の計算に寄与

析出段階の解析

I)
$$\frac{\partial C}{\partial t} + \mathbf{v} \cdot \nabla C - D\Delta C$$
$$= -B^{nucl} (C / C^{sat}, t) f(t, x, r) + \int_{r_{crit}}^{\infty} B^{diss} (C, t) n(t, x, r) dr$$
$$(A \equiv E = 71^{-12} = 4 + 5 \text{ expected operation})$$

(金属原子に関する species equation)

$$(\mathbf{I}) \quad \frac{\partial n(t, x, r)}{\partial t} + \mathbf{v} \cdot \nabla_x n(t, x, r) + \frac{\partial}{\partial r} (n(t, x, r) \cdot \mathbf{R}) = b(t, x, r)$$

(粒子に関する population balance equation)

 $C: 金属原子濃度 <math>B^{nucl}:$ 核発生速度 $B^{diss}:$ 核溶解速度 n:粒子の密度分布関数 f:発生した核の密度分布関数 R: 成長速度

現在のところ完全なモデル化には至っておらず



拡散層の制御例-回転電極(RDE)



$$\gamma \ll 1$$
$$v_r = r\omega \left(a\gamma - \frac{\gamma^2}{2} - \frac{1}{3}b\gamma^3 + \cdots\right)$$
$$v_y = (\omega v)^{1/2} \left(-a\gamma^2 + \frac{\gamma^3}{3} + \frac{1}{6}b\gamma^4 + \cdots\right)$$

ω: 電極の回転速度

動粘度

v:

a = 0.51023 b = -0.6159

$$\gamma \to 0 \quad (y \to 0)$$

 $\gamma: \gamma = \left(\frac{\omega}{\nu}\right)^{1/2} y$

$$v_r = 0.51 \ \omega^{3/2} v^{-1/2} r \ y$$

 $v_y = -0.51 \ \omega^{3/2} v^{-1/2} y^2$
拡散層の制御例-回転電極(RDE)

拡散層(濃度プロファイル)の計算





拡散層(濃度プロファイル)の計算



$$\frac{\partial^2 C}{\partial y^2} = -\frac{y^2}{B} \frac{\partial C}{\partial y}$$

$$\downarrow$$

$$C(y) = \left(\frac{\partial C}{\partial y}\right)_{y=0} \int_0^y \exp\left(-\frac{y^3}{3B}\right) dy$$

$$v_r = 0.51 \ \omega^{3/2} v^{-1/2} r \ y$$
$$v_y = -0.51 \ \omega^{3/2} v^{-1/2} y^2$$

$$\lim_{y \to \infty} C(y) = C^* = \left(\frac{\partial C}{\partial y}\right)_{y=0} \int_0^\infty \exp\left(-\frac{y^3}{3B}\right) dy$$

$$= \left(\frac{\partial C}{\partial y}\right)_{y=0} 0.8934 \ (3B)^{1/3}$$

$$\therefore \quad C(y) = \frac{C^*}{0.8934 \ (3B)^{1/3}} \int_0^y \exp\left(-\frac{y^3}{3B}\right) dy$$

拡散層の制御例-回転電極(RDE)

拡散層(濃度プロファイル)の計算



拡散層/濃度プロファイルがωによって生じる流れによって制御

拡散層の制御例-回転電極(RDE)

拡散層(濃度プロファイル)の計算



 $v_{r} = 0.51 \omega^{3/2} v^{-1/2} r y$ $v_{y} = -0.51 \omega^{3/2} v^{-1/2} y^{2}$ 電流値がωによって生じる流れによって制御

Discussion with Prof. Dr. Dieter Bothe



<u>流路内における</u> <u>速度分布は放物線状である</u>



Discussion with Prof. Dr. Dieter Bothe

速度分布は粒子によって影響を受けない



Discussion with Prof. Dr. Dieter Bothe



Discussion with Prof. Dr. Dieter Bothe

